Alarm Management and Operator Graphics

Peter Andow Honeywell Process Solutions

for

Institution of Chemical Engineers Southampton, May 2005



Agenda

Alarm Management

- Awareness: "The Alarm Management Problem"
- Progress to Date
- What Next?
- Operator Graphics
 - Experience
 - ASM Guidance
 - Applications

Summary

Problem Awareness ...

Honeywell

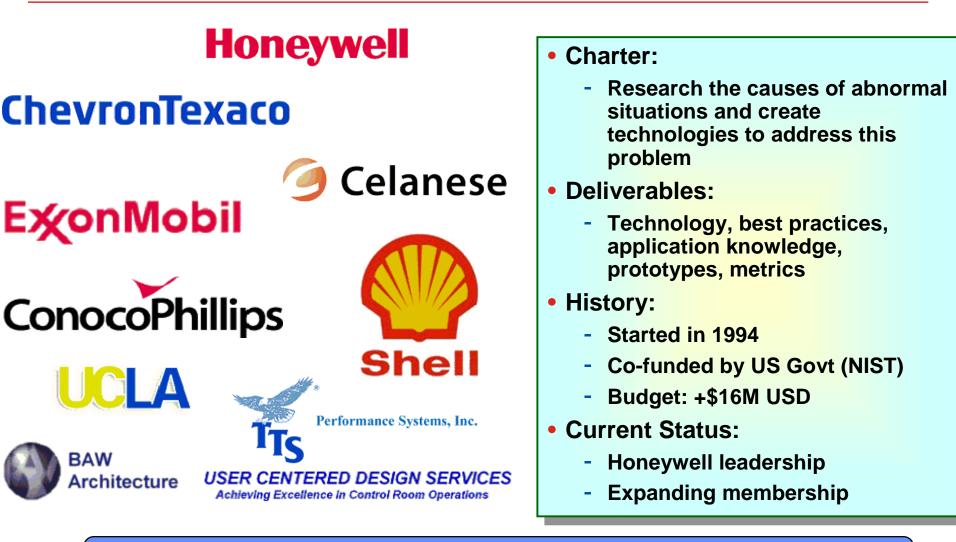


More recently ...

Honeywell



ASM Consortium



Customer Driven Solution Drives 3-8% Additional Capacity

No plant-wide philosophy and guidelines for alarms

Major operating upsets generate alarm "floods"

Minor operating upsets generate significant numbers of alarms Documentation and graphics support varies widely

Some alarms "stand" for long periods of time When nothing is wrong, there are active alarms

Alarm configuration management is poor

Alarm Prioritization is inconsistent

Alarm activations occur without need for operator action

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Forces Driving Honeywell Alarm Solutions

Honeywell

ASM Consortium

- "Effective Alarm Management Practices" document

Honeywell Customers

- Shell ESP
 - "We know our limits and we operate within those limits all the time."

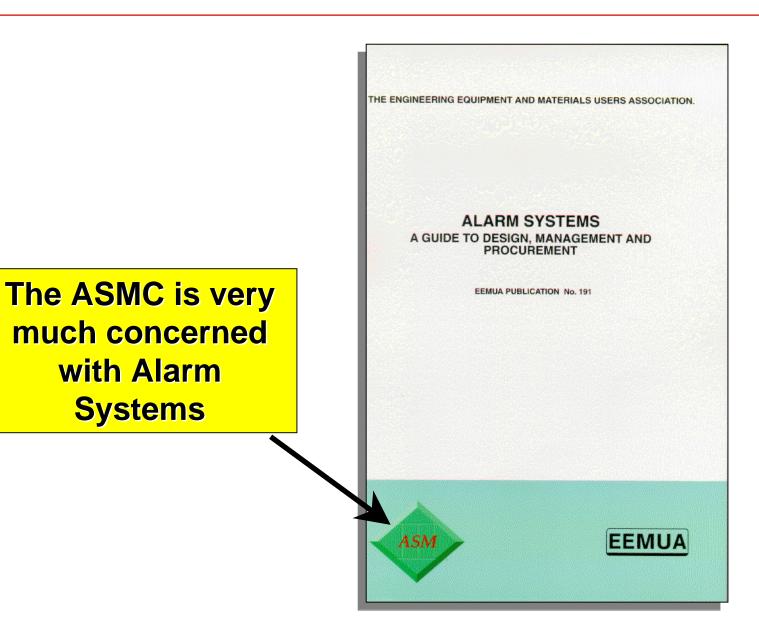
- ExxonMobil

- Mutual Development Funding
- Others...
- EEMUA 191
 - "The de facto standard"
- Standards
 - IEC 61508/61511
 - UK HSE Document
 - OSHA 1910.119
 - Etc.

HSE. Better alarm han		E information sheet
The 1994 explosion and fires at the Texaco Mildrof Haven refinery injured heenty-six people and caused damage of around £48 million and significant production loss. Key factors that emerged from the Health and 324fey Executive's (HSEs) investigation' were: • There were too many alarms and they were poorly prioritised. • The control room displays did not help the operators to understand what was happening. • There had been inadequate training for dealing with a stressful and sustained plant upset. In the last 11 minutes before the explosion the two operators had to recognise, acknowledge and act on 275 alarms. The should read this guidance and why the information sheet gives simple and practical donate to manger, supervisors on two to recognise and deal with hypical human-factor oblems involving any system in the behenkal and liked notaties. It aims to prevent future accidents additors to and given the Ergoperent additors. It haves to prevent future accidents additions. It haves to prevent future accidents additions to manger to any end practical additions to manger to any end practical additions. It aims to prevent future accidents additions. It aims to prevent future accidents additions to the addition to any end ments.	STEP 1: FNF Are there proble: Take some measu • How many ala • Are they all nee (Note process obsignated as • How many star Asson of the minute the first many soci • How many star Asson operators an every ten minute the first ten minute ten	THE ENGINEERING EQUIPMENT AND MATERIALS USERS ASSOCIATION. BALARM SYSTEMS A GUIDE TO DESIGN, MANAGEMENT AND PROCUREMENT LEINUA PUBLICATION No. 191
kpproach iere is a step-by-step approach for improving alarm anding; as with managing any other risk: frstly, identify my problems; secondly, plan what to do; and thirdly, liminate or control them.	 Is clear help av How easy is it t Are the terms u operators use? 	ASM

EEMUA ... "the de-facto standard"





EEMUA 191

- A huge step forward!
- Heavy focus on redesign ("rationalisation"):
 - Removal of meaningless "alarms"
 - Better use of priorities (e.g. for use during floods):
 - ~ 5% URGENT
 - ~ 10% HIGH
 - ~ 85% LOW
 - Wider limits "alarms" not useful for minor deviations
 - More effective use of existing alarm configuration parameters
- Targets for activation frequency
- EEMUA also calls for other improvements which are often neglected (MOC, alarm suppression etc.)

The Three Common Problems

Problem Type	Solution Approach	Target (e.g. from EEMUA) (one operator)		
Standing alarms	Mode-based alarming. Shelving.	< 10		
Background alarms	Alarm rationalisation (just "Bad Actors" ?)	< 10 per hour		
Alarm floods	Full alarm rationalisation. Enhanced processing.	< 10 in first 10 minutes of upset		

ASM Consortium Alarm System Performance Metrics Benchmarking Project



Alarms/10 mins (ASM ® Consortium Data)

Honeywell Very Likely 10.0 **Unacceptable** 9.0 8.0 7.0 6.0 EEMUA 5.0 Rating 4.03.02.01.0 **Very Likely** 0.0 Low – Average – High Alarm Rate for 40 Consoles Acceptable

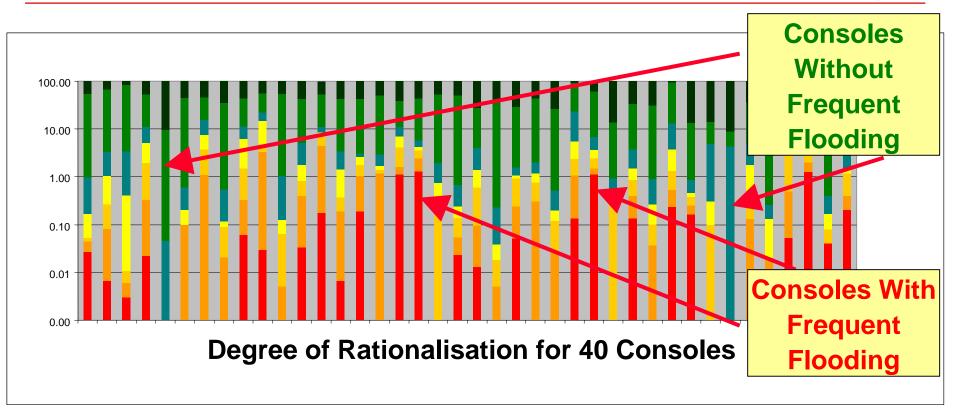
- Average alarm rates (the "background" rate) have improved
- Sites can meet and sustain the EEMUA targets ("Manageable" or "Very Likely Acceptable")

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Peak Alarm Rates (ASM Consortium Data)

Honeywell



- The peak alarm rate is not closely correlated with the degree of rationalization
- Peak alarm rates exceeding 100 alarms per 10 minute window were experienced at least once by 60% of the consoles

Three Problems Summary

			Honeywell
	Tools and		
Problem Typ	progress	roach	Target
			(e.g. from EEMUA)
	<u> </u>		(one operator)
Standing alarms	Mode-based alarm	< 10	
		derable	
Background alarms -	7110	gress	< 10 per hour
	"Bad Actors .,		
Alarm floods	Full alarm rationali	< 10 in first 10	
	Ced process		minutes of upset
	The most difficu	lt	
	problem		

- As noted in the EEMUA Guide:
- Most process plant alarms are DCS-based and are covered by the International Standard IEC 61508.
- Many countries expect compliance with IEC 61508.
- According to the standard, an alarm system is safety-related if:
 - It is a claimed part of the facilities for reducing risks from hazards to people to a tolerable level
 - AND ... the claimed reduction in risk provided by the alarm system is "significant"
- "Significant" means a claimed Average Probability of Failure on Demand of less than 0.1/demand

• Terminology!!!

- If an alarm system is considered as a safety-related system then:
 - It should be designed, operated and maintained in accordance with IEC 61508.
 - It should be <u>independent and separate</u> from the process control system (unless the process control system is itself safety-related and conforms to IEC 61508).
- Many plants use (or claim to use!) a separate, <u>high-reliability</u> system for safety-related alarms.
- The traditional DCS (including Honeywell ones) are NOT engineered to IEC 61508 specifications and should NOT be used for safety-related alarms.

IEC 61511

... generally reinforces the generic requirements of IEC 61508 as far as process industry alarms are concerned



- <u>"It should be noted that a risk reduction of up to a factor of 10 might be claimed without the need to comply with IEC 61511</u>. Where such claims are made, the human factor issues will need to be carefully considered"
- "Any claims for risk reduction from an alarm should be supported by a documented description of the necessary response for the alarm and that there is sufficient time for the operator to take the corrective action and assurance that the operator will be trained to take the preventive actions"

IEC 61511

- An alarm system can be used as a method of risk reduction by reducing the demand rate on the SIS providing:
 - the sensor used for the alarm system is not used for control purposes where loss of control would lead to a demand on the SIF.
 - the sensor used for the alarm system is not used as part of the SIS.
 - limitations have been taken into account with respect to risk reduction that can be claimed for the BPCS and common cause issues.
- Some plants seem to be unaware of the IEC 61508/61511 guidance or mistakenly believe that they are following it

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Summary

More Work Required?

- So ... some incidents have raised awareness and EEMUA has given us a framework to move forward
- A lot of work has been done ...
- ... but significant problems remain:
 - Many plants have considerably improved their performance ... but <u>large</u> variations between the best and the worst (even within the same site and/or company)
 - The ASMC study (and anecdotal evidence) has shown that alarm floods are still a <u>major</u> problem
 - Rationalisation can be time-consuming and expensive ... lots of interest in better techniques/tools
 - Safety-Related alarms are a source of real concern
- Need for effective tools (not just analysis tools) and the work-process

Shell ESP Program

Operations Management Pro is the Productization of Shell ESP

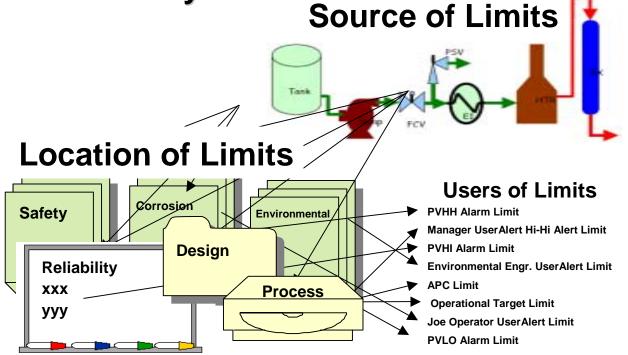
- Ensure Safe Production is a Shell Global Solutions initiative to establish work processes to...
 - <u>Establish Limits</u> for plant operations -- based on equipment, health, safety, and environmental concerns/regulations
 - assure consistency across application disciplines
 - Validate daily operating targets against these limits
 - Monitor and control deviations
 - monitor and report deviations
 - common approaches for notifying appropriate plant personnel
 - Learn and Improve -- assess plant performance
 - common end of shift logs
 - drill-down plant level access
 - deviation and alarm system metrics
- Joint Shell / Honeywell development
- Currently being installed at the 9 US Shell refineries



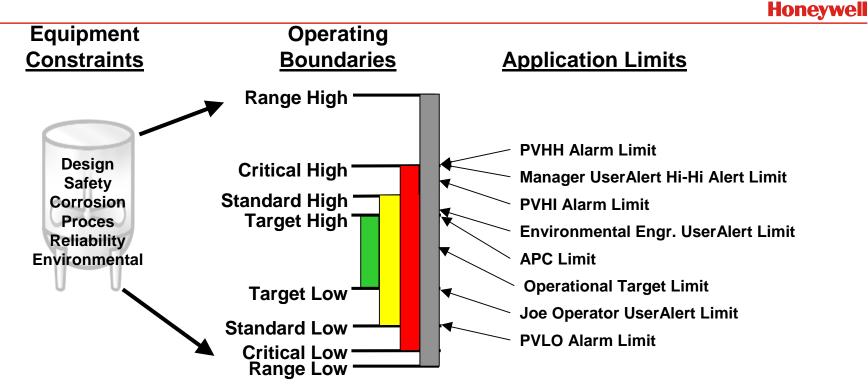
Major commitment by Shell - \$11M

Safe Operating Boundaries

- Operating within safe operating boundaries is key to safety. Many major incidents have been attributed to operations unknowingly or knowingly running outside safe operating boundary
- Boundaries are often not well documented and maintained today



Boundary Management



- Consistent reference point based on facts, documented and available to the entire operating team and other applications
- Thorough PHA, HAZOP, and alarm system design with cross functional team
 - Clear definition of safe upper and lower limits (OSHA 1910.119)
 - Identify what to monitor (alarms, alerts, production targets)
 - Capture and make available knowledge from PHA, HAZOP, AOA, other processes

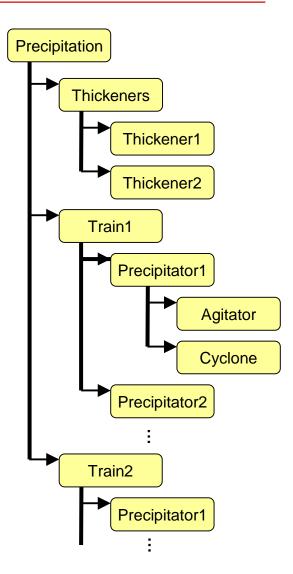
Experion Enterprise Model

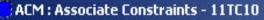
• What is the Enterprise Model?

- Allows organization of Experion platform to reflect structure of the plant including assets and boundaries
- Will become the basis for other models/views that reflect other aspects of the enterprise

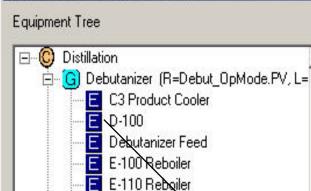
Applications organized around the hierarchical asset model

- Existing area-based mechanisms enhanced to work with more richly structured asset model
- More effective integration since application parameters are based on the same core enterprise model









T-100

D-200

T-200

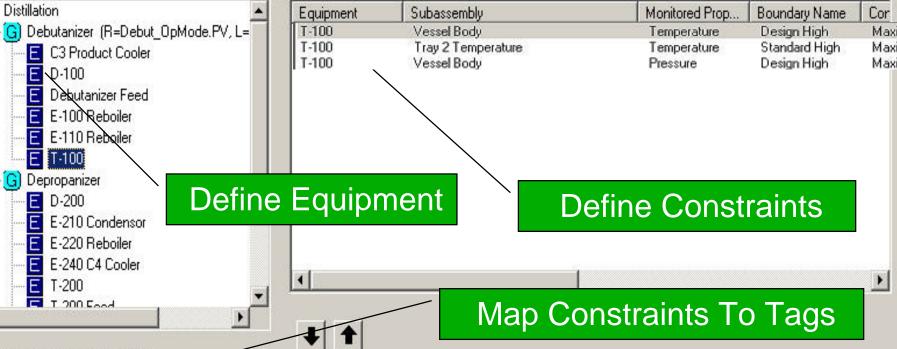
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Available Constraints not associated with 11TC10



Constraints Associated with 11TC10

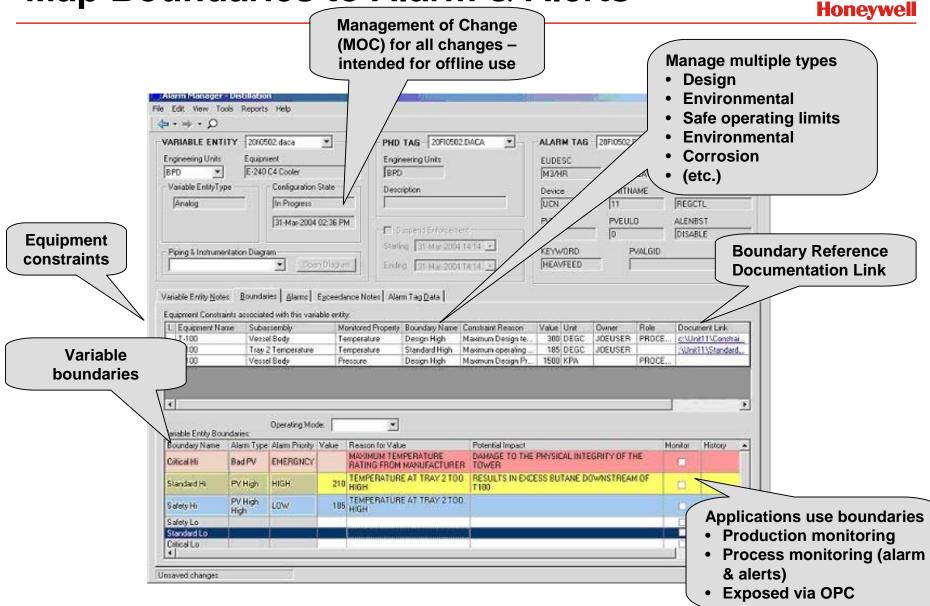
Equipment	Subassembly	Monitored Prop	Boundary Name	Constraint Reas	Value	Units	Use
T-100	Vessel Body	Temperature	Design High	Maximum Desig	300	DEGC	JOE
T-100	Tray 2 Temperature	Temperature	Standard High	Maximum opera	185	DEGC	JOE
T-100	Vessel Body	Pressure	Design High	Maximum Desig	1500	KPA	



.

Cancel

Map Boundaries to Alarm & Alerts



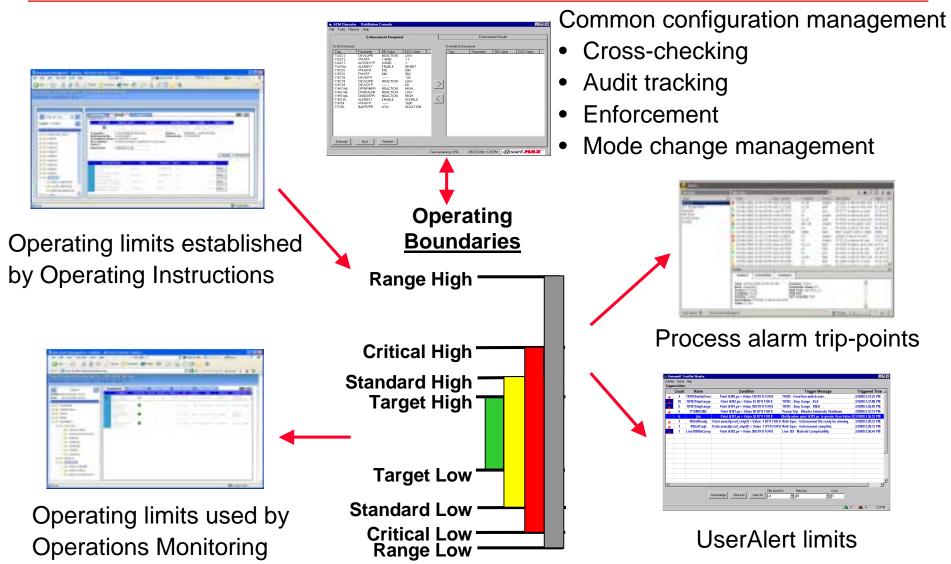
Boundary Information Availability

• ACM Information exposed:

- Boundary Values and Alarm Limits (operating mode aware)
- Alarm Help
- Alarm Documentation
- Uses:
 - GUS & HMI Web Displays
 - OI/OM Integration
 - UserAlert boundary alerts
 - APC model constraints
 - Etc

Common Database for Managing Limits

Honeywell



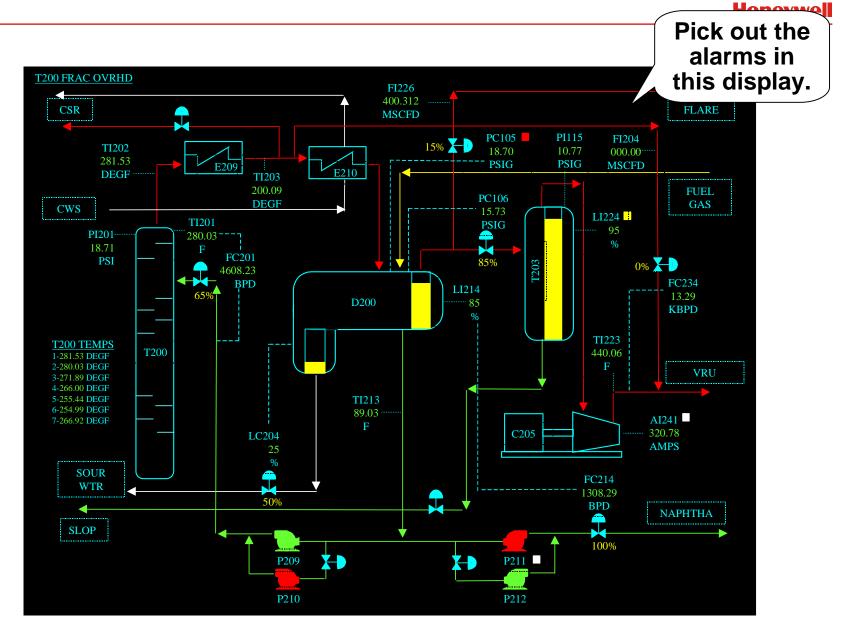
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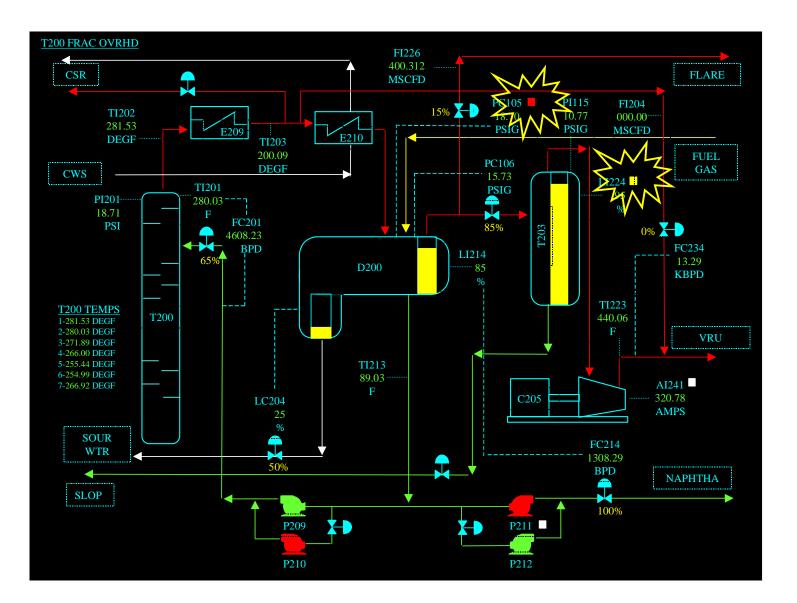
An "effective" graphic?



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An "effective" graphic?

Honeywell



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ASM Consortium Guidelines "Effective Operator Display Design"

(Version 4.00 19/June/2002)



ASM Guidance

- The detailed guidance is only available to ASM Consortium members
- Honeywell project teams can also use the guidance on non-ASM Consortium projects
- But some parts derive from public-domain information ...

Level 1: Process Area Overview Displays

- Level 1 graphics show the broadest available view of the facilities under the operator's control.
- Primary purpose is to provide situational awareness of the operators entire span of control
- Summarized on a limited number of displays.
- Contains multiple units, with the process values or safety signals being read-only from a control perspective.
- The operator is not allowed to execute any control from this display.
- Simplified process flow diagrams of a whole plant area.
- Often a combination of KPI values, trends and alarms

Level 2: Process Unit Overview Displays

- Main control interface for performing routine operational tasks
- One for every major process unit
- Enough information to control plant under normal conditions
- Allows operators to perform common tasks without changing graphics
- Used to provide information regarding key elements of the process unit

Level 3: Detailed Displays

- Exhaustive in their detail and contain all available information of smaller pieces of the process unit.
- All control loops (?) and indicators are shown on the Level 3 displays.
- Used for detailed investigations and interventions that are not time-critical.
- May also be used to show detailed alarm information (e.g. PVLL)

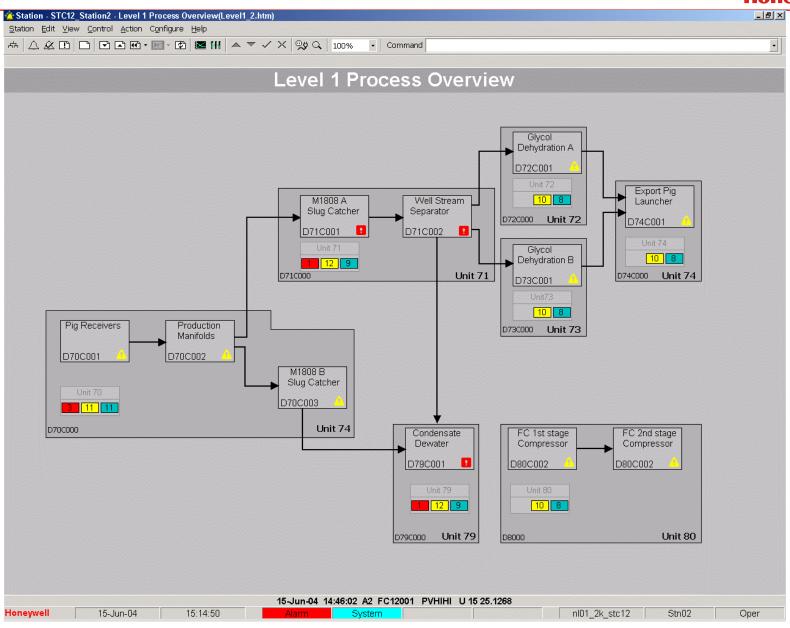
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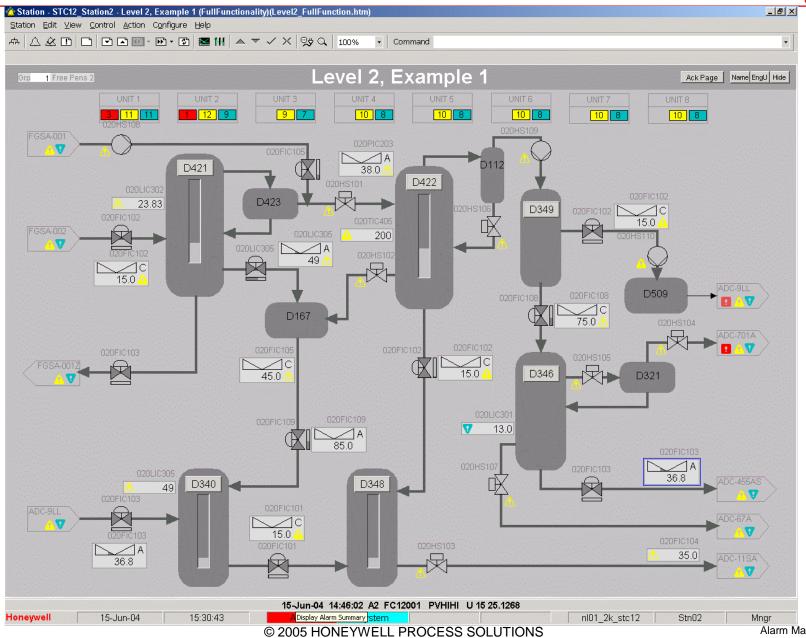
Summary

Level 1 example



Level 2 Example

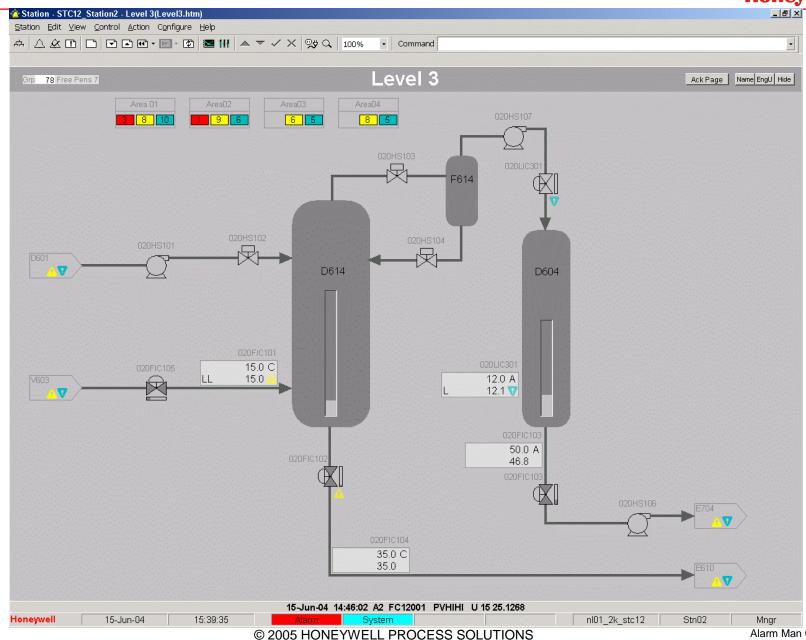
Honeywell



Alarm Man Op Graphics

Level 3 Example

Honeywell

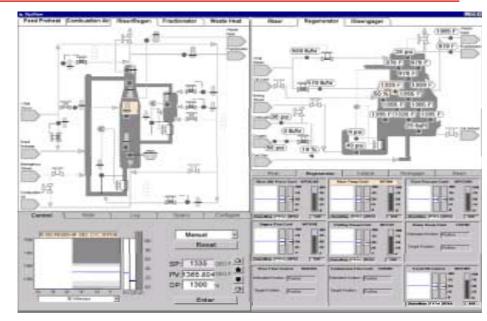


Alarm Man Op Graphics

Nova Chem, Joffre, Alberta

Honeywell

- By using the ASM concepts in one of their process units
 - ASM graphics
 - Alarm management
 - Etc ...
- >35% improvement in recognizing process deviations before an alarm
- 25% improvement in their ability to solve the problem
- 35-48% improvement in operator response time to deviations
- As compared to other units that were using US station type technologies as their control room environment, operators were able to orient to problems faster, more completely resolve the problems, and generally deal with abnormal situations faster



~ C\$1M per year in savings

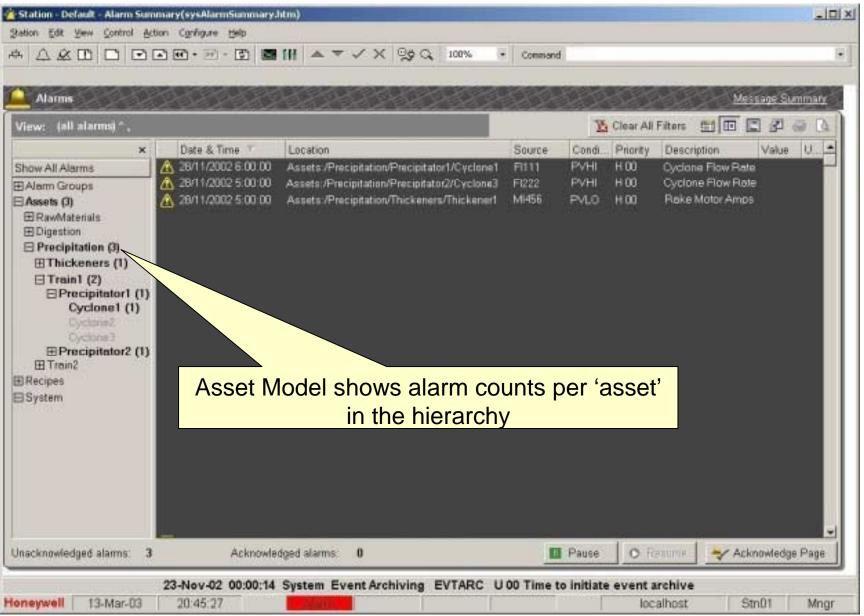
Honeywell is also applying the EEMUA guidance and ASM Graphics guidance to it's Alarm Summary as well as in the HMIWeb Solution Pack



Experion PKS Alarm Summary

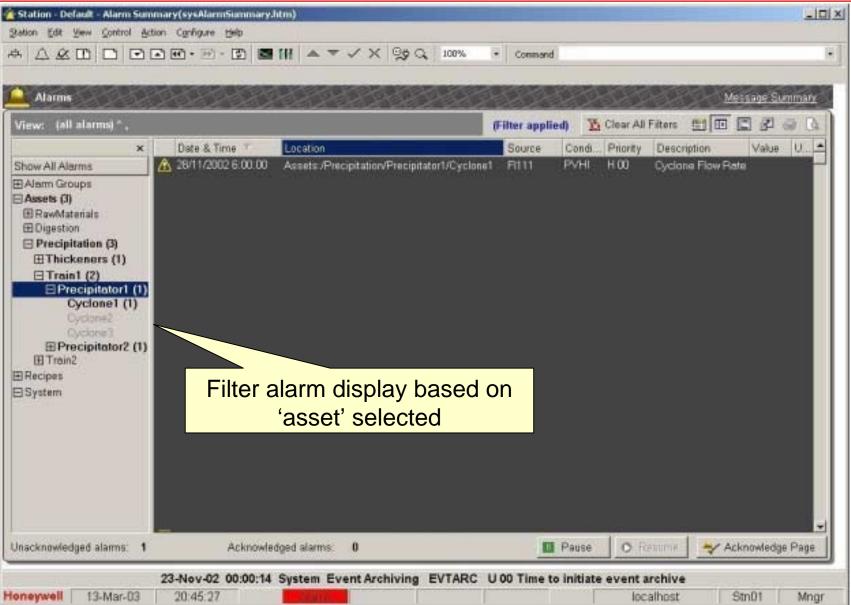
🤶 Alarms				
All areas	User/iew		· <u>*</u> # 🗉	🗄 🗗 🎒
Areas X All areas S1 - System Area	 Time Area 18-Feb-2000 10:44:43 PM Gene 18-Feb-2000 10:44:43 PM Wet B 	FIC2001 HI_HA U	· • • • • • • • • • • • • • • • • • • •	Value 🖌 🔺 177.35 m 56.19 m3
Generator Wet Ends Cooling Tower	18-Feb-2000 10:44:45 PM Coolin 18-Feb-2000 10:45:06 PM Coolin	FIC3777 LO L LIC8034 HI L	ow FIC3777 is below Lo Limit Irgent LVL8034 is above Hi Limit	12.33 m/s 99.45 m3
Auxilary	 18-Feb-2000 10:45:12 PM Gene 18-Feb-2000 10:46:12 PM Auxila 18-Feb-2000 10:46:13 PM Wet B 	TIC3215 DEV_HI U	ligh FIC1001 is above HiHi Limit Irgent TIC3215 Hi Deviation Limit ow FIC1001 is above Hi Limit	45.35 m/s 12.00 Dei 40.35 m/s
	 18-Feb-2000 10:46:13 PM Gene 18-Feb-2000 10:47:13 PM Wet B 18-Feb-2000 10:48:13 PM Auxila 	LI4006 HI U	Irgent 14006 is above Hi Limit Irgent TICS2	OPEN 129.03 m
Create and store "views" of areas,	18-Feb-2000 10:49:14 PM Gene 18-Feb-2000 10:55:14 PM Wet I 18-Feb-2000 10:55:15 PM Gene	FIC2001 HI H	ligh LIC30 One-click so ligh FIC2001 is above Hi Limit ow FIC1001 is above Hi Limit	rting! 140.35 m 35.35 m/s
filters, and sorting	 18-Feb-2000 10:55:18 PM Gene 18-Feb-2000 10:55:18 PM Gene 18-Feb-2000 10:55:18 PM Gene 	FIC1001 HI_HI H FIC1004 LO H	ligh FIC1001 is above HiHi Limit ligh FIC1004 is below to Limit	,1
	Details ×			
	General Instructions C	omments 🖣		
	Time: 18 Feb 2000, 10:01:22 PM Area: Generator Source: FIC2001 Condition: HI_HI Priority: Urgent Description: FIC2001 is above Hi Value: 6.19m	Previous: 5.93m Parameter Name: PV Help Text: See OP6.1.3 Help File: OPC Severity: 500 Hi limit	Enter commer on alarms for I analysis!	
Total alarms: 41 Total unacknowledged: 2		Presents instructions for each alarm	Pause 🛇 Resume	r- 😽 🗸

Alarm Summary

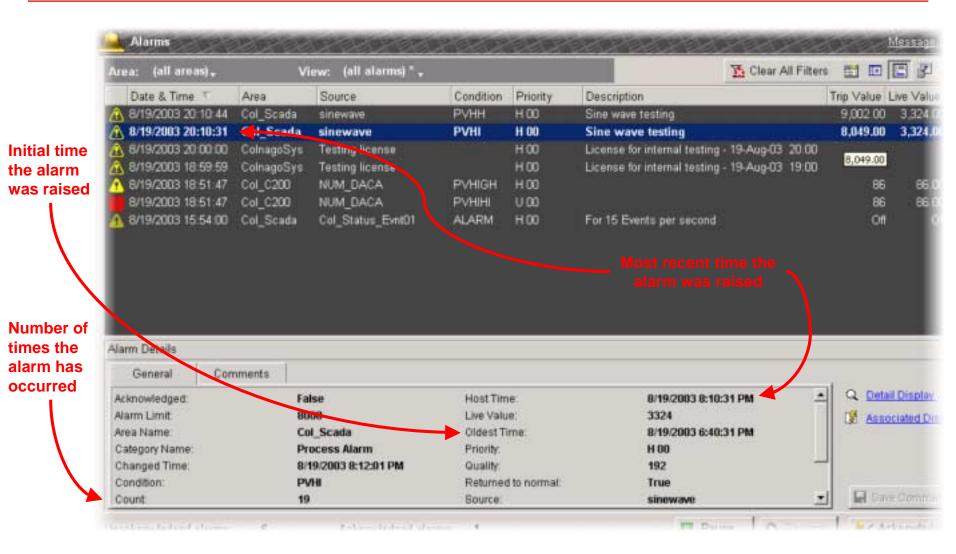


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Alarm Summary Filtering



Repeated Alarm Handling



Summary

- Considerable progress has been made in Alarm Management, particularly since the publication of the EEMUA 191 guidance.
- Safety Regulators and Insurers are also giving added momentum throughout the world.
- But much remains to be done, particularly in the area of "alarm floods".
- The use of an Asset Model and associated work processes gives a promising way forward.
- Operator Graphics vary enormously in effectiveness. Good graphics give real benefits.
- The ASM Consortium has it's own guidance in both areas – being applied extensively in Experion PKS.

Contact Information

peter.andow@honeywell.com





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